ACID BUFFERING CHARACTERISTICS OF ACID MINE DRAINAGE 1/2 200 3

OOI MEI HONG

DISSERTATION SUBMITTED IN PARTIAL FULFILLMENT OF THE REQUIREMENTS FOR THE DEGREE OF BACHELOR OF SCIENCE WITH HONOURS

PERPUSTAKAAN UNIVERSITI MALAYSIA SABAM

PROGRAMME INDUSTRIAL CHEMISTRY SCHOOL OF SCIENCE AND TECHNOLOGY UNIVERSITY MALAYSIA SABAH

MAY - 2010



UNIVERSITI MALAYSIA SABAH	TA SAR
BORANG PENGESAHAN STATUS TESIS@ JUDUL: Acid Buffering chamateristics of acid mine drainage.	•-
IJAZAH: IJAZAH JARJANA MUNA JANS DENGAN KEPUJIAN (KIMIA ZNOUSTR)	
SAYA OUT MEI HONG SESI PENGAJIAN: 2007/2008 (HURUF BESAR)	
mengaku membenarkan tesis (LPSM/Sarjana/Doktor Falsafah) ini disimpan di Perpustakaan Universiti Malaysia Sabah dengan syarat-syarat kegunaan seperti berikut:-	
 Tesis adalah hakmilik Universiti Malaysia Sabah. Perpustakaan Universiti Malaysia Sabah dibenarkan membuat salinan untuk tujuan pengajian sahaja. Perpustakaan dibenarkan membuat salinan tesis ini sebagai bahan pertukaran antara institutsi pengajian tinggi. Sila tandakan (/) 	
SULIT (Mengandungi maklumat yang berdarjah keselamatan atau Kepentingan Malaysia seperti yang termaktub di dalam AKTA RAHSIA RASMI 1972)	
(Mengandungi maklumat TERHAD yang telah ditentukan oleh organisasi/badan di mana penyelidikan dijalankan)	
Disahkan Oleh NURULAIN BINTI ISMA IINIVERSITI MALAYSIA SABAH (TANDATANGAN PENULIS) (TANDATANGAN PENULIS) Disahkan Oleh NURULAIN BINTI ISMA LIBRARIAN (TANDATANGAN PENULIS)	IL BAH
Alamat Tetap: 44, Lengtolc Mya Tanbong, 11060, Ayer <u>Itan, Rubu Pinang</u> Nama Penyelia	
Tarikh: 7 May 2010 . Tarikh: 7.5.2010	
 CATATAN:- *Potong yang tidak berkenaan. **Jika tesis ini SULIT atau TERHAD, sila lampirkan surat daripada pihak berkuasa /organisasi berkenaan dengan menyatakan sekali sebab dan tempoh tesis ini perlu dikelaskan sebagai SULIT dan TERHAD. @Tesis dimaksudkan sebagai tesis bagi Ijazah Doktor Falsafah dan Sarjana secara penyelidikan atau disertai bagi pengajian secara kerja kursus dan Laporan Projek Sarjana Muda (LPSM). 	
PERPUSTAKAAN UMS	



•

ī

į

۰.



DECLARATION

I hereby declare that the materials in this thesis is my own except for quotations, excerpts, equations, summaries and references, each of which have been fully acknowledge.

OOI MEI HONG (BS07110497)

12 April 2010



VERIFICATION

Signature

1. SUPERVISOR (PROF. DR. MARCUS JOPONY)

han

EXAMINER 1
 (Dr. Noumie Surugau)





4. DEAN (PROF. DR. MOHD. HARUN ABDULLAH)

leager



ACKNOLEDGEMENT

First and foremost, I would like to express my sincere gratitude towards my supervisor, Prof. Dr. Marcus Jopony for his valuable advice, guidance, support, perseverance, motivation and help throughout the dissertation. On the other hands, I would like to thank Mr. Mohd Recheidy Mohd Rashid, the lab assistant for his help throughout the lab work providing all the necessary apparatus and chemicals. Besides, I also appreciate the Mr. Jerry who providing me with the apparatus and chemicals required. Furthermore, I truly appreciate the guidance from Mr. Wong Hai Fatt. I would like to thank all my supportive friends for their helping hands. Many thanks are to my family members for their undying love and emotional support. I am also grateful to all who are not mention but have help in this research a successful one. Last but not least, not forgetting to express my sincere thank to School of Science and Technology for providing the opportunity as well as the amenities to enable this research carried out successfully.

Ooi Mei Hong BS07110497 April 2010



ABSTRACT

Acid mine drainage (AMD) samples, AMD S1 and AMD S2, from Mamut Copper Mine (MCM), Ranau, Sabah were investigated for its acid buffering characteristics by potentiometric titration with NaOH. The AMD has the following characteristics: $pH\sim2.56$, total acid= 343-365 mg CaCO₃/L, dissolved Fe= 2.4-2.5 mg/L, Mn= 11.3-11.9 mg/L, Cu= 4.4-4.5 mg/L, Zn= 2.6-2.7 mg/L, Al= 3.1 mg/L. For comparison, acidified distilled water as well as Fe(III) and Al(III) solutions were also tested. The results showed that acidified distilled water exhibited a gradual increase in pH with increasing amount of base added. Comparatively, Fe(III) and Al(III) solutions required higher amount of base to attain pH 7.0, and this increased with the concentration of Fe(III) and Al(III). In the case of AMD, a much higher amount of base was required to raise its pH to 7.0. This can be attributed to the strong buffering at pH 3.5-5.0, which was more apparent than those exhibited by the Fe(III) and Al(III) solutions.



ABSTRAK

Sampel saliran asid lombong (AMD), AMD S1 dan AMD S2 dari Lombong Tembaga Mamut (LTM), Ranau, Sabah telah dikaji ciri-ciri penimbalan asid secara titratan potensiometrik dengan NaOH. AMD mempunyai ciri-ciri berikut: pH~2.56, keasidan jumlah= 343-365 mg CaCO₃/L, kepekatan logam Fe= 2.4-2.5 mg/L, Mn= 11.3-11.9mg/L, Cu= 4.4-4.5 mg/L, Zn= 2.6-2.7 mg/L, Al= 3.1 mg/L. Air suling berasid, serta larutan Fe(III) dan Al(III) juga dikaji untuk tujuan perbandingan. Hasil kajian menunjukkan bahawa air suling berasid menunjukkan peningkatan pH yang berperingkatan dengan amaun bes yang ditambahkan. Larutan Fe(III) dan Al(III) pula memerlukan amaun bes yang lebih tinggi untuk mencapal pH 7.0 dan ini meningkat dengan kepekatan Fe(III) dan Al(III). Untuk kes AMD, amaun bes yang diperlukan untuk mencapal pH 7.0 adalah jauh lebih tinggi dan ini dapat dikaitkan dengan penimbalan pH di pH 3.5-5.0, magnitud peningkatan pH ini lebih ketara berbanding larutan Fe(III) dan Al(III).



LIST OF CONTENTS

TITLE	E PAGE	i
DECL	ARATION	II
VERI	FICATION	
ACKN	IOWLEDGEMENT	iv
ABST	RACT	v
ABS7	TRAK	vi
⊔ST	OF CONTENTS	vii
LIST	OF TABLES	xi
LIST	OF FIGURES	xii
LIST	OF SYMBOLS AND ABBREVIATIONS	xiii
CHA	PTER 1 INTRODUCTION	1
1.1	Mining and the Environment	1
1.2	Acid Mine Drainage in Sabah	3
1.3	Objectives of Study	3
1.4	Scope of Study	4
СНА	PTER 2 LITERATURE REVIEW	5
2.1	Acid Mine Drainage Formation and Characteristic	5
	2.1.1. Oxidation of Pyrite	5



Page

	2.1.2	Factors Affecting Acid Generation During Pyrite Oxidation	8	
	а.	Effects of pH	8	
	b.	Effects of oxygen concentration	10	
	C.	Effects of bacteria	10	
	d.	Effects of particle size of pyrite	11	
	e.	Presence of carbonate minerals	11	
	f.	Effects of the type of sulphide mineral	12	
	2.1.3	Oxidation of other sulphide minerals	13	
	2.1.4	Dissolution of mineral matrices	14	
	2.1.5	Characteristics of AMD	14	
2.2	Enviro	onment Impacts of AMD	17	-
	2.2.1	Effects on water quality	17	JRIVER
	2.2.2	Effects on aquatic life	18	PERPU
2.3	Total	Acidity of AMD	20	ISTAKA IALAYS
	2.3.1	Mineral Acidity	21	
2.4	Neutr	alization of AMD	24	
	2.4.1	Neutralization Process	24	
	2.4.2	Buffering ability of AMD	28	
CHA	PTER 3	METHODOLOGY	32	
3.1	Aque	ous Samples	32	
	3.1.1	Acid mine drainage samples	32	
	3.1.2	Acidified Distilled Water	32	
	3.1.3	Aqueous solutions of Fe(III)	32	
	3.1.4	Aqueous solution of AI(III)	33	
	3.1.5	Preparation of NaOH Solution	33	



	2.1.2	Factors Affecting Acid Generation During Pyrite Oxidation	8	
	а.	Effects of pH	8	
	b.	Effects of oxygen concentration	10	
	C.	Effects of bacteria	10	
	d.	Effects of particle size of pyrite	11	
	e.	Presence of carbonate minerals	11	
	f.	Effects of the type of sulphide mineral	12	
	2.1.3	Oxidation of other sulphide minerals	13	
	2.1.4	Dissolution of mineral matrices	14	
	2.1.5	Characteristics of AMD	14	
2.2	Enviro	nment Impacts of AMD	17	ja na sector de la companya de la co
	2.2.1	Effects on water quality	17	JRIVER
	2.2.2	Effects on aquatic life	18	PERPU NSITI M
2.3	Total	Acidity of AMD	20	STAKA
	2.3.1	Mineral Acidity	21	
2.4	Neutra	alization of AMD	24	
	2.4.1	Neutralization Process	24	
	2.4.2	Buffering ability of AMD	28	
CHAI	PTER 3	METHODOLOGY	32	
3.1	Aque	ous Samples	32	
	3.1.1	Acid mine drainage samples	32	
	3.1.2	Acidified Distilled Water	32	
	3.1.3	Aqueous solutions of Fe(III)	32	
	3.1.4	Aqueous solution of Al(III)	33	
	3.1.5	Preparation of NaOH Solution	33	



3.2	Determ	nination of Physico-chemical Characteristics	33
	3.2.1	рН	33
	3.2.2	Total acidity	33
	3.2.3	Fe, Mn, Cu and Zn	34
	а.	Instrumentation	34
	b.	Preparation of standard solutions	35
	С.	Preparation of calibration curve	35
	d.	Analysis of samples	36
	3.2.4	Aluminium	36
	a.	Preparation of aluminium stock solution	36
	b.	Preparation of H_2SO_4 solution	36
	с.	Preparation of ascorbic acid solution	36
	d.	Preparation of buffer reagent	37
	e.	Preparation of dye stock solution	37
	f.	Preparation of AI standard solutions	37
	g.	Analysis of sample	38
3.3	Pote	ntiometric Titration	38
	3.3.1	Titration of AMD samples	38
	3.3.2	2 Titration of Fe(III) Solutions	3 9
	3.3.3	3 Titration of AI(III) Solutions	39
	3.3.4	Titration of acidified distilled water	39
CHA	PTER	4 RESULTS AND DISCUSSION	41
4.1	Phys	sico-chemical characteristics of AMDs from Mamut Copper Mine	41
	4.1.	1 pH	41
	4.1.	2 Total acidity	42



	4.1.3	Dissolved metals (Fe, Mn, Cu, Zn, and Al)	42
4.2	Acid b	uffering characteristics	43
	4.2.1	Acidified distilled water	43
	4.2.2	Fe(III) solutions	44
	4.2.3	Al(III) solutions	45
	4.2.4	AMD S1 and AMD S2	47
CHAF	PTER 5	CONCLUSION	51
REFE	RENCI	ES	52
APPE	APPENDIX		



LIST OF TABLES

.

Page

Table 2.1	Common carbonate minerals in mine overburden, listed in descending order of their capability to neutralize acid	12
Table 2.2	Acid-producing sulphides and non-acid-producing sulphides	12
Table 2.3	Acid production according to the type of acid producing sulphides	13
Table 2.4	Characteristics of AMDs from various types of mine and locations	15
Table 2.5	Water quality data of selected AMD impacted rivers/streams	16
Table 2.6	Major effects of AMD	18
Table 2.7	Biological effects of metals on fish	19
Table 2.8	Chemical compounds used in AMDs treatment	26
Table 2.9	pH range for the formation of metal precipitate	28
Table 3.1	Standard conditions and characteristic concentration checks for atomic absorption spectrometer, AAS	34
Table 3.2	Concentrations range of standard solutions prepared according to metal	35
Table 4.1	Concentration of dissolved metals in AMD samples	43
Table 4.2	Concentration of dissolved metals in decreasing order	43
Table 4.3	No. of moles of NaOH used in potentiometric titration to achieve pH 7.0 for acidified distilled water and standard solution of Fe(III)	44
Table 4.4	No. of moles of NaOH used in potentiometric titration to achieve pH 7.0 for acidified distilled water and standard solution of Al(III)	46
Table 4.5	No. of moles of NaOH used in potentiometric titration to achieve pH 7.0 for acidified distilled water, AMD S1 and S2	48



LIST OF FIGURES

Figure 1.1	Mamut Copper Mine in Ranau, Sabah	3
Figure 2.1	The simplified diagram illustrating reaction pathways for pyrite oxidation	7
Figure 2.2	Yellow boy in a stram receiving acid drainage from surface coal mining	8
Figure 2.3	Oxidation rate of ferrous iron (Fe ²⁺) to ferric iron (Fe ³⁺) as a function $pH(p_{m}=0.20 \text{ bar})$	9
Figure 2.4	Solubility diagram of which is dependent on pH	10
Figure 2.5	Acidic components of the water samples	24
Figure 2.6	Measured titration curve of the acidic lake water and composition of the precipitates; the grey shades denote the different buffering	31
Figure 4.1	sections pH values of AMD samples	41
Figure 4.2	Average of total acidity of AMD samples	42
Figure 4.3	Titration curves for acidified distilled water and standard solutions	43
Figure 4.4	or re(III) Titration curves for acidified distilled water and standard solutions of Al(III)	46
Figure 4.5	Titration curve for AMD S1	48
Figure 4.6	Titration curve for AMD S2	48



:

ABBREVIATIONS AND SYMBOLS

~	nearly to/ about
<	less than
>	more than
AAS	Atomic absorption spectrophotometer
Al	Aluminium
AMD	Acid mine drainage
Cu	Copper
Eq	Equation
Fe	Iron
MCM	Mamut Copper Mine
Mn	Manganese
TDS	Total dissolved solids
Zn	Zinc
E _c	Electrical conductivity
mg/L	Milligram per liter
ppm	Part per million
mg/ml	Milligram per mililiter
mg CaCO ₃ /L	Milligram calcium carbonate per liter
µS/cm	Microsiemens per centimeter
µg/L	Microgram per liter
K _{sp}	Solubility product
%	Percent
mmol L ⁻¹	Milimole per liter
μm	micrometer
µm/ml	micrometer per mililiter
nm	nanometer
mL	mililiter
NaOH	Sodium hydroxide
H ₂ O ₂	Hydrogen peroxide
HCI	Hydrochloric acid
H ₂ SO ₄	Sulphuric acid
CaCO ₃	Calcium carbonate
OH.	Hydroxide
H*	proton
H ₂ CO ₃	Carbonic acid
Fe(III)	Iron(III)
Al(III)	Aluminium(III)



CHAPTER 1

INTRODUCTION

1.1 Mining and the Environment

Mining is a process where valuable minerals or other geological materials from the earth are extracted, usually from ore bodies or veins. The industry provides the impetus to open up new lands, creating towns, providing numerous jobs to the local population and improvements of basic infrastructures (Sengupta, 1993). Locally, mining has an important place in the annals of Malaysia's development and presently it is one of the important income earners for the country (Wu, 1999).

Mining, like other industrial activities, however have negative impacts to the surrounding environment. The deleterious effects include deposition of huge amounts of solid wastes including mine tailings (Dudka and Adriano, 1997), contamination of soils by heavy metals (Ciccu *et al.*, 2003), turning land into a useless wasteland, and



PERPUSTAKAAN MAIVERSITI MALAYDIA destruction of aquatic life (Swift, 1982). In fact, many present-day problems are associated with abandoned historical mines (Banks *et al.*, 1997).

One of the most common and significant post-mining environmental problems is acid mine drainage, AMD (Gray, 1997). Typically, AMD is characterized by low pH, high acidity, high TDS, high conductivity, high sulfate and elevated concentration of heavy metals (Singh 1987; Gray 1998; Nordstrom *et al.*, 2000; Bell *et al.*, 2001).

Inputs of AMD can have adverse effects on the receiving water quality. Typically, AMD-impacted rivers have acidic pH, low alkalinity, high TDS, sulphate and dissolved metals (Filipek *et al.*, 1987; Sengupta, 1993; Nordstrom *et al.*, 2000; Shaver *et al.*, 2006). This has lead to various environmental problems. Therefore, AMD need to be treated prior to discharge.

One of the treatment methods for AMD is neutralization using alkaline or calcareous materials (i.e. to increase the pH to near 7). This neutralization process, however, is not as simple and easy as it may seem. It can be hindered by the low solubility of the alkaline or calcareous materials as well as the significant presence of dissolved metals in the AMD (Younger *et al.*, 2002; Hammarstrom *et al.*, 2003; Hedin, 2006). The dissolved metals, in particular Fe and AI, will contribute towards mineral acidity, which in turn enables the AMD to resist the changes in pH during neutralization. Consequently, the efficiency of a neutralization process can be dependent on the characteristics of the AMD.



1.2 Acid Mine Drainage in Sabah



Figure 1.1 Mamut Copper Mine in Ranau, Sabah.

The Mamut Copper Mine in Ranau, Sabah (Figure 1.1) ceased operation in 1999. During its operational phase, various environmental issues have been reported (Murtedza *et al.*, 1985; Jopony & Murtedza, 1994). Like other abandoned mines elsewhere, this mine left behind a legacy of AMD problem. Presently, AMD at this mine area are left untreated. As a result, several rivers in the area are showing signs of AMD pollution.

1.3 Objectives of Study

The objectives of the study are:

 To determine the changes in pH of the local acid mine drainage (AMD) during neutralization process.



(ii) To determine the effect of dissolved heavy metals (Fe and Al) in solution on neutralization process.

1.4 Scope of Study

This study focused on the changes in pH of AMD samples collected from Mamut Copper Mine, in Ranau Sabah during neutralization process. The significance of dissolved metals (Fe and AI) in the neutralization process is further investigated using acidic aqueous solutions containing varying concentrations of Fe and AI.



CHAPTER 2

LITERATURE REVIEW

2.1 Acid Mine Drainage Formation and Characteristics

AMD is a widespread environmental issue resulting from the oxidation of sulfide minerals on to exposure to both oxygen and water. There are various types of sulfide minerals but pyrite, marcasite and pyrrhotite are perhaps the most common sources of AMD production. The oxidation process result in the production of iron- and aluminium- rich sulphuric acid solutions with high levels of trace metals (Singer and Stumm 1970; Drever 1997).

2.1.1 Oxidation of Pyrite

The oxidation of pyrite, FeS_2 , can involve the following reactions (Eq. 2.1-2.4) (Singer & Stumm, 1970; Sengupta, 1993; Evangelou, 1995):

Oxidation of pyrite by O_2 :

 $2FeS_2 + 7O_2 + 2H_2O \longrightarrow 2Fe^{2+} + 4SO_4^{2-} + 4H^+$ (2.1)



Oxidation of
$$Fe^{2^+}$$
 by O_2 :
 4Fe^{2^+} + O_2 + 4H⁺ ---> 4Fe³⁺ + 2H₂O
 (2.2)

 Precipitation Of Fe^{3^+} :
 5

 Fe³⁺ + 3H₂O ---> Fe(OH)₃ + 3H⁺
 (2.3)

 Oxidation of pyrite by Fe^{3^+} :
 5

 FeS₂ + 14Fe³⁺ + 8H₂O ---> 15Fe²⁺ + 2SO₄²⁻ + 16H⁺
 (2.4)

The first important reaction is the oxidation of the sulfide mineral in the presence of oxygen. The mineral is oxidized into dissolved ferrous iron (Fe^{2+}), sulfate and hydrogen (Eq. 2.1). The dissolved ferrous iron (Fe^{2+}) as well as the sulfate (SO_4^{2-}), and the two moles of hydrogen ions represent an increase in the total dissolved solids and total acidity of water. If the environment is sufficiently oxidizing, which is dependent on O_2 concentration, pH and bacteria activity, much of the liberated ferrous iron (Fe^{2+}) will be oxidized to ferric iron (Fe^{3+}) according to the Equation 2.2 with the consumption of acidity. Equation 2.2 is the rate-determining step in pyrite oxidation as the conversion of ferrous iron to ferric iron is slow at pH below 5 under abiotic conditions.

The ferric iron (Fe³⁺) formed (Eq. 2.2) will remain in solution if the pH maintain below 3.5. It however, undergoes hydrolysis and precipitation as the pH > 3.5. The precipitation as into ferric hydroxide (Fe(OH)₃) simultaneously lowering the pH (Eq. 2.3) by producing three moles on hydrogen ions.

Any Fe³⁺ which does not undergo precipitation from solution can oxidize additional pyrite (Eq. 2.4), generating much greater amounts of ferrous iron, sulphate, and acidity.





Figure 2.2: Yellow boy in a stream receiving acid drainage from surface coal mining. Source: Hardesty (2005)

2.1.2 Factors Affecting Acid Generation During Pyrite Oxidation

The primary factors determining the rate of acid generation during pyrite oxidation include oxygen concentration and solution pH (Smith and Shumate, 1970), the presence of *Thiobacillus* bacteria (USEPA, 1971), particle size (McKibben & Barnes, 1986), presence of carbonate minerals, and type of sulphide mineral.

a. Effects of pH

The kinetics of oxidation of ferrous iron which can occur either abiotically or biotically, is dependent on pH. According to Stumm and Morgan (1996), the kinetic of the oxidation can be represented as follows:

 $\frac{-d[Fe^{2^+}]}{dt} = k[Fe^{2^+}][OH^-]p_{O_2}$

The oxidation rate is independent of pH at low pH. On the contrary, at higher pH (>5) the second order dependence on [OH⁻] is apparent (Figure 2.3).



Figure 2.3: Oxidation rate of ferrous iron (Fe²⁺) to ferric iron (Fe³⁺) as a function pH ($p_{02} = 0.20$ bar).

Also, the hydrolysis reaction of iron depends on total Fe^{3+} and pH as well. Under equilibrium conditions, only a negligible concentration of dissolved ferric iron exist at pH 3 (Figure 2.4).





Figure 2.4: Solubility diagram of Fe(OH)₃ which is dependent on pH. Source: Stumm & Morgan (1981)

b. Effect of oxygen concentration

Oxidation of pyrite only occurs in the presence of both water and oxygen. Oxygen plays the role as the terminal electron acceptor by oxidation of ferrous iron (Fe^{2+}) to ferric ion (Fe^{3+}) (Evangelou & Seta, 1999). The rate of pyrite oxidation will rise when the concentration of oxygen increase. This leads to more generation of acid. Hence, it can be concluded that the overall rate of pyrite oxidation is dependent on the oxygen concentration.

c. Effects of bacteria

Bacteria play a major role in accelerating the rate of acid generation. The sulfide-oxidation process is accelerated by about 100 times in the presence of *Thiobacillus* bacteria compared with an abiotic control (Mielke *et al.*, 2003).